

# Theoretical Comparative Study of CSP and PV Power Generation Systems for Remote Areas

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**Abstract:** This paper analyzes the sizing and modeling of a mini power plant using CSP (concentrated solar power) and PV (photovoltaic) technology, focusing on remote areas such as CERER in Senegal. The objective is to model a PT (parabolic trough) collector connected to an Ericsson engine following a Joule cycle in order to evaluate electricity production during a typical day in April. Two operating strategies are considered: “sun-dependent” and “fixed hours”. The research includes modeling solar energy into usable heat using a PT Solar Courant collector, then into usable heat for work. The collector is characterized by high performance, low cost, and 80% optical efficiency with a collection area of 69.24 m<sup>2</sup>. The results will enable a purely energy-based comparison, highlighting the efficiencies and collection areas between CSP and PV.

**Key words:** CSP (concentrated solar power), PV (photovoltaic), Ericsson engine, operating strategies, comparison.

## Nomenclature

### Latin Letters

Symbol	Designation	Unit	$\dot{Q}_f$	Thermal power received by the heat fluid	W
$c_{p,f}$	Specific mass heat capacity at constant pressure	J.kg <sup>-1</sup> K <sup>-1</sup>	$\dot{Q}_r$	Thermal power transmitted from the receiver to the engine heat exchanger	W
D	Hydraulic diameter of the absorber tube	m	$\dot{Q}_{ray}$	Thermal power lost by radiation	W
F	Shape factor	-	$\dot{Q}_s$	Thermal power emitted by the sun and received by the concentrator	W
$h_{conv}$	Coefficient of forced convection of the heat fluid	W.m <sup>-2</sup> K <sup>-1</sup>	$Q_{sto}$	Stored thermal energy	J
$h_v$	Coefficient of external mixed convection	W.m <sup>-2</sup> K <sup>-1</sup>	S	Fluid passage section	m <sup>2</sup>
DNI	Direct Normal Insolation	W.m <sup>-2</sup>	$S_{conc}$	Opening surface of the concentrator	m <sup>2</sup>
$l_{conc}$	Width of the concentrator	m	$S_m$	Wetted surface of the receiver tube	m <sup>2</sup>
$l_r$	Perimeter of receiver tube	m	$S_r$	Surface of receiving envelope	m <sup>2</sup>
$L_{conc}$	Length of the concentrator	m	t	Time	s
$\dot{m}$	Mass flow rate of the fluid	kgs <sup>-1</sup>	$T_0$	Ambient temperature	K
$P_m$	Wetted perimeter of the absorber tube	m	$T_{C-R}$	Compressor outlet temperature, heat exchanger inlet temperature	K
$\dot{Q}_{conc}$	Thermal power emitted by the concentrator and received by the receiver	W	$T_{E-R}$	Temperature at regulator outlet, temperature at heat exchanger inlet	K
$\dot{Q}_{conv}$	Thermal power lost by convection	W	$T_f$	Average temperature of the heat fluid in the tube	K
			$T_{f(x)}$	Local temperature of the heat fluid	K
			$T_{fus}$	Salt melting temperature	K

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$T_{in}$	Input temperature of the heat fluid in the tube	K
$T_{out}$	Output temperature of the heat fluid in the tube	K
$T_p$	Average temperature of the wall of the receiver tube	K
$T_p(x)$	Local temperature of the wall of the receiver tube	K
$T_{PT}$	Temperature output PT expansion valve input	K
$T_{PT-sto}$	Storage outlet temperature regulator inlet temperature	K
$\dot{W}_{C,i}$	Indicated mechanical compression power	W
$\dot{W}_{C,real}$	Actual mechanical compression power	W
$\dot{W}_{E,i}$	Indicated mechanical expansion power	W
$\dot{W}_{E,real}$	Actual mechanical expansion power	W
$\dot{W}_{elec}$	Electrical power generated by the alternator	W
$\dot{W}_{i,net}$	Indicated net mechanical power	W
$\dot{W}_{net}$	Net mechanical power	W

### Greek Characters

$\alpha_{conc}$	Geometric concentration ratio $\alpha_{conc} = \frac{S_{conc}}{S_r}$	-
$\alpha_r$	Absorption coefficient of the receiver tube	-
$\beta$	Pressure ratio	-
$\epsilon$	Emissivity coefficient of the receiver tube	-
$\epsilon_R$	Recovery efficiency	-
$\zeta_{conc}$	Geometrical efficiency of the concentrator	-
$\kappa_{PT}$	Effective efficiency of the PT	-
$\lambda$	Thermal conductivity of the fluid	$W \cdot m^{-1} K^{-1}$
$\mu$	Dynamic viscosity of the fluid	$Pa \cdot s$
$\eta_{conc}$	Optical efficiency of the concentrator	-
$\eta_{elec}$	Alternator efficiency	-
$\eta_{engine}$	Engine efficiency	-
$\eta_{meca,1}$	Mechanical compression efficiency	-
$\eta_{meca,2}$	Mechanical expansion efficiency	-
$\eta_{S-elec}$	Solar to electricity conversion efficiency	-
$\eta_{th-PT}$	Thermal global efficiency of the PT	-
$\rho_{conc}$	Optical efficiency of reflection	-
$\sigma_{SB}$	Stefan Boltzmann constant	$W \cdot m^{-2} K^{-4}$
$\tau_{conc}$	Optical efficiency of transmission	-

## 1. Introduction

The issue of sizing solar thermal power plants has been addressed in several different ways without the aim of establishing a general method [1-3].

As a high-performance clean energy source, hybrid CSP (concentrated solar power)-PV (photovoltaic) power generation delivers reliable, clean, and

continuous energy across multiple scenarios, including electricity, heating, hydrogen and oxygen production, making it ideal for high-altitude regions [4]. Hybrid concentrated solar power (CSP) and PV (photovoltaic) systems, known for clean energy attributes and robust grid-support capabilities, have emerged as a viable and cost-effective solution. The hybridization of solar PV and CSP systems has many benefits. Hybrid PV-CSP systems enable the simultaneous generation of electricity and heat, maximizing the use of solar energy, particularly in sun-rich areas like Cameroon [5]. Yu et al. [6] propose a novel Carnot Battery system based on an open-cycle ultra-high-temperature heat pump and a tower CSP (concentrated solar power) configuration. In their study, thermodynamic models for charging/discharging cycles and solar plants were established for a system with 10 MW power output and the results show that the proposed system achieves a round-trip efficiency of 56.2% under typical operating conditions, with a potential increase to 62.5% at lower discharging pressure ratio. Concentrated solar power generation is a promising technology that relies on the concentration of solar radiation to drive a heat engine and generate electricity. Fang et al. [7] are carried out an OIES (off-grid integrated energy system) combining PV (photovoltaic), CSP (concentrated solar power), TES (thermal energy storage), and EES (electrochemical energy storage) is designed to minimize both the LCoE (levelized cost of energy) and LPSP (loss of power supply probability). Scenario comparisons show that a CSP + TES configuration alone cuts LCOE by 14.17% and LPSP by 3.24%, yet causes PV curtailment. Compared to solar PV and onshore wind alternatives, CSP cannot currently compete on the levelized cost of electricity (LCoE) [8]. Also accord to Adak et al. [9], the levelized cost of energy (LCoE) of solar energy driven power systems is expected to drop  $\sim 3 \text{ \textcent/kWh}$  for utility scale solar PV and  $5 \text{ \textcent/kWh}$  for baseload CSP power plants by 2030. An

evaluation of two solar technologies—PV (photovoltaic) and PT-CSP (parabolic trough) CSP technology was conducted by Okeke et al. [10] under specific geographical and techno-economic criteria to support solar electricity and green hydrogen development across Nigeria. Their results indicate that 105.63 GWe of grid capacity is required to meet Nigeria's energy demand, whereas 57.32 GWe from grid-connected solar plants needed to replace unsustainable grid supplying 54.3% of estimated population. Almetwally et al. [11] examine the current state of solar-powered RO (reverse osmosis) desalination, focusing on technological advancements, integration strategies, and prevailing challenges. The analysis encompasses various configurations, including PV (photovoltaic) systems, CSP (concentrated solar power), and hybrid models, assessing their performance, efficiency, and applicability across different geographical contexts. CSP offers greater dispatchability and reliability by integrating TES (thermal energy storage), which allows excess thermal energy collected during the day and used at night or during peak demand [12]. CSP (concentrated solar power) equipped with integrated thermal storage offers a groundbreaking solution. It delivers dispatchable electricity and functions as a large, cost-effective thermal “battery”, making it an ideal complement to wind and PV by storing solar heat for use during nighttime or cloudy conditions [13].

We will size a mini-CSP (concentrated solar power) plant of a few dozen kWh for the CERER site in Senegal. To do this, we will model a parabolic trough collector coupled with an Ericsson open Joule cycle engine with recovery adapted to electricity production. The aim is to evaluate the electrical energy produced by a given installation of components on a typical day in April, which is the sunniest month. We will assume two operating strategies: “sun-dependent” and “fixed hours”. Next, we will compare the energy and

collection areas of CSP and PV (photovoltaic) solar energy.

## 2. Materials and Method

### 2.1. Modeling Solar Energy into Usable Heat

We will model a PT (parabolic trough) collector consisting of a cylindrical-parabolic concentrator and a linear receiver. This sensor will be referred to as the PT Solar Courant collector. To find the outlet temperature of the heat transfer fluid, which will be the working fluid temperature of the engine, we start with the energy balance equation for an elementary volume at the absorber tube (Fig. 1) [14, 15].

The PT collector operates according to the following system:

$$\left\{ \begin{array}{l} \kappa_{PT} DNI \cdot l_{conc} = h_{conv} P_m (T_p(x) - T_f(x)) \\ \quad + h_v l_r (T_p(x) - T_0) \\ \quad + \epsilon \sigma F l_r (T_p(x)^4 - T_0^4) \\ \dot{m} c_{p,f} \frac{dT_f}{dx} = h_{conv} P_m (T_p(x) - T_f(x)) \end{array} \right. \quad (1)$$

$$\dot{Q}_s = DNI S_{conc} \quad (2)$$

$$\dot{Q}_{conc} = \alpha_r \eta_{conc} DNI \cdot S_{conc} \quad (3)$$

$$\dot{Q}_r = \dot{Q}_{conc} - h_v S_r (T_r - T_0) \\ - \sigma_{SB} F \epsilon S_r (T_r^4 - T_0^4) \quad (4)$$

$$\eta_{th-PT} = \frac{\dot{Q}_r}{\dot{Q}_s} \quad (5)$$

We assume a collector that offers high performance at low cost, with proven reliability and longevity. It has high optical precision with an optical efficiency  $\eta_{conc}$  of 80% and a high level of solar tracking. The length of a module  $L_{conc}$  is 12 m by  $l_{conc} = 5.77$  m wide, giving a collection area of  $S_{conc} = 69.24 \text{ m}^2$ . It is easy for a glassmaker to reproduce. It is rigid in torsion and bending, corrosion-resistant, and can withstand winds of up to  $31.5 \text{ ms}^{-1}$  [16].

We will model a receiver tube with an outer diameter of 23 mm, giving an outer perimeter of  $l_r = 72$  mm. It has an absorbance  $\alpha_r \geq 0.95$  (rounded to 1) and an emissivity  $\epsilon \leq 0.14$ .

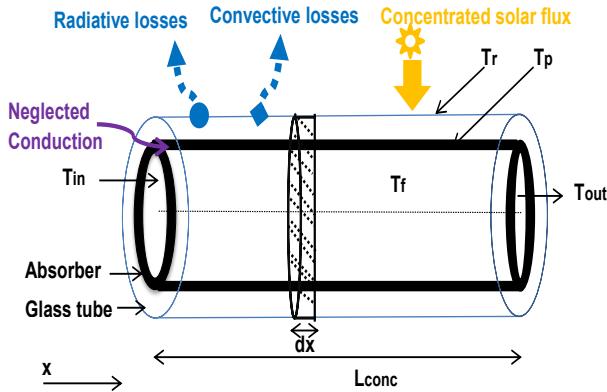


Fig. 1 Schematic diagram of the collector.

Table 1 PT Solar Courant collector specifications used for sizing.

Parameters	Values
$L_{\text{conc}}$	12 m
$l_{\text{conc}}$	5.77 m
$\alpha_{\text{conc}}$	80
$l_r$	$7.2 \cdot 10^{-2}$ m
$P_m$	$4.7 \cdot 10^{-2}$ m
$\eta_{\text{conc}}$	0.8
$\alpha_r$	1
$\varepsilon \cdot F$	0.10

Thus, the geometric concentration ratio of the sensor used for sizing will be 80. Its characteristics are summarized in Table 1.

## 2.2 Modeling Heat in Indicated Work

Using an approach similar to that of other authors [17], we consider an Ericsson engine operating according to Joule's thermodynamic cycle in an open cycle. It is a reciprocating engine with external heat input, separate compression and expansion chambers, recovery, and a single-phase gaseous working fluid. The working fluid is air, which is treated as an ideal gas with constant specific heat. The air is recycled, without renewal as in any external combustion engine, which therefore requires two heat sources. The cold source is atmospheric air and the hot source is provided in the form of heat from the parabolic trough concentrator.

The system describes a cycle of elementary transformations that we will assume to be reversible

in order to study them more easily. The Joule cycle consists of two isentropic and two isobaric processes.

The successive stages of the thermodynamic cycle are represented in a Temperature Entropy diagram (Fig. 2). The air cycle consists of an isentropic compression ( $P_{\text{max}}$ ) of atmospheric air at  $T_0$  inside the compression cylinder C ( $0 \rightarrow C-R$ ), an isobaric preheating of the air by the recuperator R ( $C-R \rightarrow R-PT$ ), an isobaric heating of the air by the parabolic trough concentrator PT ( $R-PT \rightarrow PT$ ), an isentropic expansion in the expansion cylinder E ( $PT \rightarrow E-R$ ), the isobaric transfer of heat to the recuperator R ( $E-R \rightarrow R-0$ ), and finally a return to atmospheric temperature  $T_0$ , at atmospheric pressure  $P_0$ .

We assume that the thermal power transmitted by the receiver  $\dot{Q}_r$  to the engine's heat exchanger is received in its entirety by the engine's working fluid. The recuperator R is considered to be a perfect heat exchanger, with no thermal losses. Pressure losses are not taken into account, and only the PT is diabatic.

### 2.2.1 Determination of Cycle Power and Efficiency

The equations governing the system are described below, and the engine characteristics are given in Table 2.

$$\dot{W}_{i,\text{net}} = \dot{W}_{E,i} - \dot{W}_{C,i} \quad (6)$$

$$\dot{W}_{E,i} = \dot{m}c_{p,\text{air}}(T_{PT} - T_{E-R}) \quad (7)$$

$$\dot{W}_{C,i} = \dot{m}c_{p,\text{air}}(T_{C-R} - T_0) \quad (8)$$

$$\dot{W}_{\text{net}} = \dot{W}_{E,\text{real}} - \dot{W}_{C,\text{real}} \quad (9)$$

$$\dot{W}_{C,\text{real}} = \dot{W}_{C,i}/\eta_{\text{meca},C} \quad (10)$$

$$\dot{W}_{E,\text{real}} = \eta_{\text{meca},E} \times \dot{W}_{E,i} \quad (11)$$

$$\eta_{\text{engine}} = \dot{W}_{\text{net}}/\dot{Q}_r \quad (12)$$

By introducing an alternator with efficiency  $\eta_{\text{elec}}$  mechanical energy  $\dot{W}_{\text{net}}$  will be converted into electrical energy with power  $\dot{W}_{\text{elec}}$ :

$$\dot{W}_{\text{elec}} = \eta_{\text{elec}} \times \dot{W}_{\text{net}} \quad (13)$$

$$\eta_{\text{S-elec}} = \dot{W}_{\text{elec}}/\dot{Q}_s \quad (14)$$

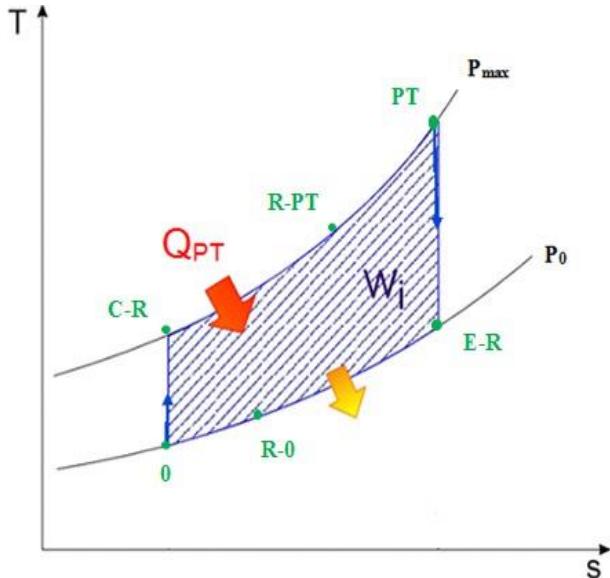


Fig. 2 (T, S) diagram of the Joule cycle with heat recovery.

Table 2 Ericsson engine specifications used for sizing.

Parameters	Values
$\eta_{meca,C}$	0.9
$\eta_{meca,E}$	0.9
$\varepsilon_R$	0.8

### 3. Results and Discussions

#### 3.1 Production "Sun-Dependent"

For solar power generation, the load curve is not fixed; you choose when to generate electricity and at what load. It should be noted that in hot regions, peaks in electricity demand often coincide with peaks in sunlight. In this case, the design of a solar installation requires knowledge of: the nature of the installation and the solar irradiation at the installation site [14, 15]. The thermodynamic cycle will be variable and the high temperature of the cycle will continue to change throughout the day depending on the irradiation.

We will first look at the evolution of the TPT collector outlet temperature over time (Fig. 3).

The temperatures obtained are generally satisfactory, reaching over 1,200 K.

Using the same principle, the instantaneous electricity production and the efficiencies of the collector  $\eta_{th-PT}$  and the engine  $\eta_{engine}$  (Fig. 4) evolve with the selected flow rate and pressure ratio.

Like the temperature of the fluid at the collector outlet, the electrical power  $\dot{W}_{elec}$  varies with time and therefore with the DNI, which is the key factor in concentration systems. With this sensor, we also note that its thermal efficiency varies between  $\sim 57\%$  and  $\sim 72\%$ . It should be remembered that the ideal energy efficiency that this collector could achieve is  $\eta_{th-PT} = \eta_{conc} = 80\%$ , with the absorption coefficient of the receiver tube being  $\alpha_r = 1$ . However, we can see that the engine efficiency  $\eta_{engine}$  varies little over time, and is generally between 10% and less than 14%. This collector is quite powerful and could be used with other more powerful thermodynamic cycles.

With this study, we were also able to calculate the average efficiencies of the collector  $\eta_{th-PT} = 70\%$  and the engine  $\eta_{engine} = 13\%$ .

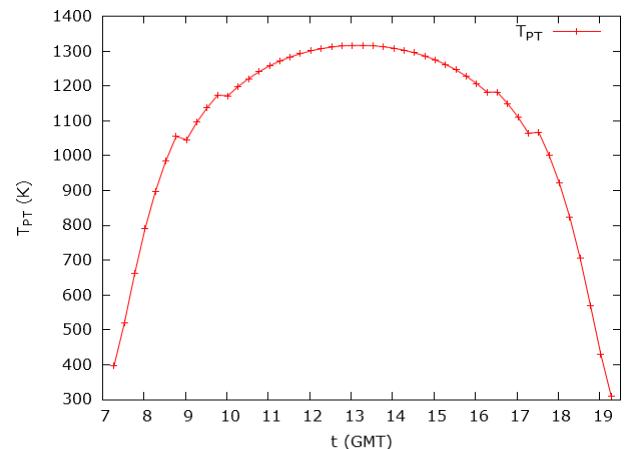


Fig. 3 Change in the output temperature of the TPT collector over time.

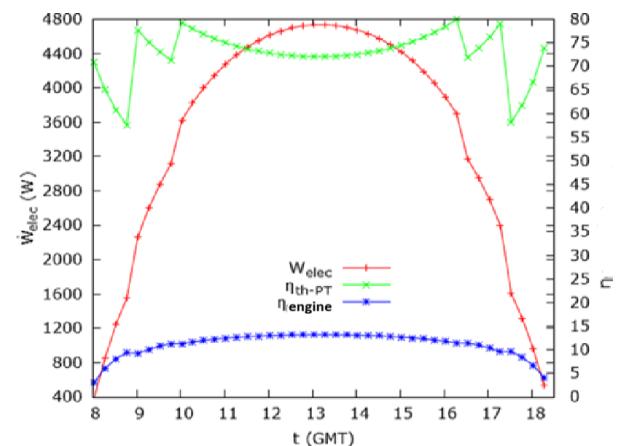


Fig. 4 Instantaneous optimal electricity production and evolution of the efficiencies.

### 3.2 Production at "Fixed Hours"

For production at set times, the charging or discharging curves will be fixed. The site's energy requirements must be known. The integration of thermal storage will provide a permanent source of heat. The high temperature of the cycle will be constant and equal to the outlet temperature of the storage  $T_{PT-sto}$ . With this collector, we will size up the thermal storage load to deduce the overall daily production. We will use Table 3 to obtain the daily irradiation.

Regardless of the engine, we are primarily interested in the amount of heat stored. The storage is such that during production, we will always have a mixture of solid and liquid to remain in a phase change state and have the  $T_{PT-sto}$  temperature equal to the melting temperature of the salt  $T_{fus} = 716$  K. It is important to remember its latent heat of fusion  $L_f$ , which is  $-241,000$  J.kg $^{-1}$ .

On a typical day in April, the daily DNI is 6,690 W.h.m $^{-2}$ .day $^{-1}$ . The surface area of the concentrator  $S_{conc} = 69.24$  m $^2$  receives thermal energy  $Q_s = 463,215.6$  W.h.day $^{-1}$  from the sun per day. With an optimal thermal efficiency  $\eta_{th-PT}$  of 70% for the collector and assuming that there are no heat losses between the receiver and the storage system, the amount of heat stored with the collector would be 324,250.9 W.h.day $^{-1}$ . This thermal energy  $Q_{sto}$  will enable the salt to be brought from the ambient temperature  $T_0$  to the melting temperature  $T_{fus}$  (in the form of sensible heat) and to remain there (in the form of latent heat).

$$Q_{sto} = m_{salt}c_{p,salt}(T_{fus} - T_0) + m_{salt}L_f \quad (15)$$

with:  $m_{salt}$  is the mass of the storage salt to be determined and  $c_{p,salt}$  is its heat capacity.

The heat capacities of salts are often determined experimentally, or estimated and weighted based on the molar fraction of their components. In general, the thermal capacity of molten salts varies little with temperature. The specific heat capacity  $c_{p,salt}$  of the eutectic mixture of sodium chloride and magnesium chloride salts (NaCl/MgCl $_2$ ) at 42% mol MgCl $_2$  is 1,087 J.kg $^{-1}$ K $^{-1}$ .

To store a quantity of heat  $Q_{sto}$  of 324,250.9 W.h.day $^{-1}$ , a minimum mass of salt  $m_{salt}$  of 1,684 kg is required, i.e., a volume of approximately  $\sim 1$  m $^3$  with the density of liquid NaCl/MgCl $_2$ , which is 1,680 kg.m $^{-3}$ . It should be noted that these salts are very inexpensive.

With the aim of always having a mixture of solid and liquid in storage, only part of the latent heat will be used to generate electricity (i.e., a maximum of 112,731 Wh). We will consider an engine with an efficiency of 12% (with a high cycle temperature of  $T_{fus} = 716$  K; the engine's performance will be revised downwards) coupled with an alternator with an electrical efficiency of 90%. The maximum total electrical energy  $W_{elec}$  that could be produced during a typical day in April would then be 12,175 W.h. The solar-to-electric conversion efficiency would then be  $\eta_{S-elec} = 2.63\%$ . We note that this efficiency is low; without storage, the efficiency was 7.7%. In fact, there is a penalty incurred by storage because, as we have seen Fig. 2, the outlet temperature of the fluid from the collector often exceeds  $T_{fus} = 716$  K. However, if we had used the heat produced by the collector directly, we would have had a higher cycle temperature than  $T_{fus}$  and therefore more electricity (Fig. 5). The high temperature of the cycle is a direct factor in electrical power. However, the advantage of storage remains the ability to anticipate production, given that solar resources are highly unpredictable. To offset the penalties incurred by storage, we can consider a control loop that allows for simultaneous storage and production, using storage as a last resort.

Under the same operating conditions, we extrapolate to determine the daily production for all other months of the year (Table 3).

With production at fixed times via storage, the energy produced is generally slightly above 10 kWh, except in July, August, and September (the rainy season). This constraint can be circumvented by integrating hybridization with another energy source.

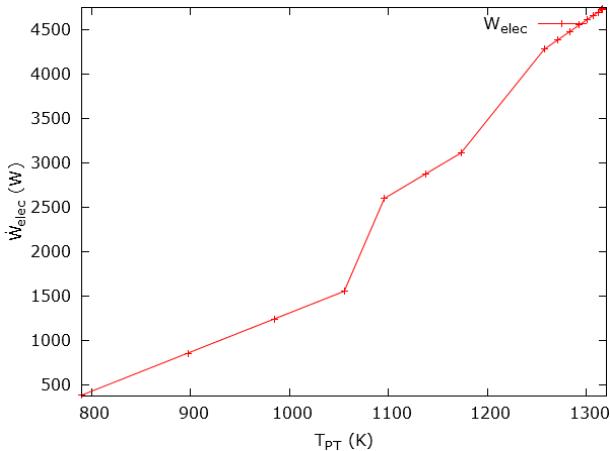


Fig. 5 Evolution of electrical power  $\dot{W}_{elec}$  as a function of temperature  $T_{PT}$ .

Table 3 Daily electricity production.

Month	$\dot{Q}_s$ (kWh/day)	$\dot{W}_{elec}$ (kWh/day)
January	404.4	10.63
February	436.9	11.48
March	481.9	12.66
April	463.2	12.18
May	490.2	12.88
Jun	446.6	11.74
July	366.9	9.64
August	326.1	8.57
September	331.6	8.72
October	415.4	10.92
November	427.2	11.23
December	412.7	10.85
Average	416.8	10.95

### 3.3 Comparison with Photovoltaic Systems

Due to its modularity and ease of operation, photovoltaics are gaining ground over CSP for small to medium-sized installations.

Less popular and less mature than photovoltaic solar energy, CSP is nevertheless more advantageous, especially for medium and large installations. However, above a certain power level, photovoltaic and CSP will be in direct competition [18, 19]. But where should we draw the line between medium and high power? To confirm the advantage of CSP over PV for medium power, we will conduct a comparative study of our thermodynamic system and the MACSEN-PV project's pilot PV plant located at the CERER center.

This pilot facility is intended to serve as:

- A technology demonstration platform for this type of facility;
- A test bed for the various operating conditions that may be encountered in the Senegalese electricity grid;
- A teaching aid for the training of local technicians.

With a power output of 3.15 kW<sub>p</sub> it consists of 18 polycrystalline silicon cell modules covering a total area of 23.4 m<sup>2</sup>. It has a room equipped with two inverters. The first (3.2 kW) is a grid-connected inverter that generates alternating current from the photovoltaic modules. The second (2.2 kW) generates current from the batteries and starts up in the event of a grid failure. It is also used to charge the battery bank (capacity (C10) per unit: 816 Ah). The room is also equipped with measurement and control systems.

The purpose of our theoretical comparison between CSP and solar PV is purely energetic and not economic. To do this, we will reduce the surface area of the PV modules to the same surface area as the solar field of the collector, i.e., 69.24 m<sup>2</sup>. Thus, with a 90% efficiency injection inverter and 80% module efficiency, the electrical power delivered by a surface area of 69.24 m<sup>2</sup> would be:  $\dot{W}_{elec} = 6.7$  kW, i.e., a solar-to-electric conversion efficiency of 9.7%.

To determine the electrical power of our CSP system for comparison purposes, we will use the same STC (standard test conditions) as for PV, i.e., AM1.5 spectrum under 1,000 W/m<sup>2</sup> irradiance and an ambient temperature of 25 °C or 298 K. With more consistent sunlight, we used a pressure ratio of  $\beta = 7$  and an air flow rate of  $\dot{m} = 0.02$  kg s<sup>-1</sup>. The electrical power delivered would then be  $\dot{W}_{elec} = 12.3$  kW with a thermal efficiency of the collector  $\eta_{th-PT} = 76.9\%$  and a solar-to-electric conversion efficiency of  $\eta_{s-elec} = 25.6\%$ . This result is unequivocal and proves that CSP is more promising than photovoltaics. It has been proven that PV requires much more space and has a lower conversion efficiency: in the case of PV, commercial cells have an efficiency of 12% to 15%, while CSP has an efficiency of around 20% [18, 19].

Currently, CPV (concentrated photovoltaics), a niche technology, is revolutionizing the solar energy market. According to the German Fraunhofer ISE (Institute for Solar Energy) Systems and the American NREL (National Renewable Energy Laboratory), the price of CPV modules is expected to fall by 2030 to a level competitive with conventional modules. Recently, the market has been moving towards Micro-CPV (miniaturization of components to reduce costs) and hybrid systems combining photovoltaic and thermal energy [20]. Regardless of the technology used, the main input factor remains sunlight, and it offers a reliable solution for energy generation in the sunny regions where we live.

#### 4. Conclusion

In this study, we designed a mini power plant with a capacity of around 10 kW using two different approaches. Regardless of the method used, solar energy remains highly unpredictable, and the hourly distribution of sunlight is the key factor in electricity production. The most influential factors are also electricity demand and installed capacity. However, we cannot comment on the price of solar thermal electricity due to the lack of a market. This study also allowed us to confirm that storage, although beneficial for smoothing and forecasting production, remains a penalty from an energy perspective. In general, a basic solar field module must be sized, and for the rest, the number of modules required per row must be added. The comparison between solar PV and solar CSP allowed us to see the advantages of the latter, particularly in terms of space savings and efficiency.

Although the results obtained depend on the performance of certain parameters relating to the characteristics of the collector and engine, they are acceptable and realistic. The technologies modeled and dimensioned are feasible. These results now need to be validated experimentally.

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